



# Deterioration of long-serving cement-based sandcrete structures in Nigeria

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## Abstract

The fall in living standard of the Nigerian citizenry, starting from the mid-1980s, has encouraged massive importation of secondhand goods, most especially industrial machines, cars, motorcycles, etc. It is a well-known fact that the majority of these equipment are very inefficient and produce a lot of pollutants ( $\text{Cl}^-$ ,  $\text{SO}_2$ ,  $\text{CO}_2$ ,  $\text{CO}$ ,  $\text{N}_2\text{O}$ , etc), particularly as a result of incomplete fuel combustion. The presence of these pollutants has contributed not only to the depreciation of the people's quality of life, but also to the degradation of cement-based structures' physicochemical, mechanical and aesthetic qualities. This paper is aimed at developing a deterministic model, based on a mechanism of cement corrosion, to predict the deterioration of cement-based structures in Nigeria. The developed model equation showed that intensive diffusion of pollutants takes place within 0- to 10-mm-depth of the sandcrete block. It represents the relationship between concentration of pollutant and depth of their penetration and gives a comparative measure of the ease of diffusion of the latter into the structure at various depths. Variation in the type of pollutant and possible reaction, including leaching need to be considered in order to develop an acceptable model. © 2002 Elsevier Science Ltd. All rights reserved.

**Keywords:** Pollutants; Kinetics; Degradation; Hydration products; Diffusion

## 1. Introduction

The compressive strength of cement-based structures is expected to increase steadily with age. However, this statement may not be true for many structures, especially those serving in aggressive environments. In some areas, most cement-based structures were found to develop micro-cracks within a few years after construction, despite the fact that acceptable standards were observed. It has been proved by various researchers that long exposure of cement-based structures to aggressive medium containing acids, alkalis and salts immensely enhance their physicochemical and mechanical properties' deterioration [1].

Results of various researchers have shown that the weak point in hardened cement microstructure remains the presence in it of soluble and reactive  $\text{Ca}(\text{OH})_2$  [2]. Much work has been done in investigating the mechanism of various destructive processes responsible for cement-based structure deterioration [2–4]. In his work [2], Moskvic formulated the basic points for developing the theory of cement-based structure deterioration. It was established that in order to

qualitatively assess the kinetics of corrosion process, it is necessary to study the internal diffusion of an aggressive substance, the formation on the cement-based structure surface, layer of the reaction products, crystallization of corrosive components and products of their interaction with hardened cement minerals in the voids and other processes. This paper is aimed at developing a deterministic model equation based on the mechanism of cement corrosion to predict the deterioration of cement-based sandcrete commonly used as a building material in Nigeria.

## 2. Mathematical modelling of pollutants' diffusion into sandcrete structure

The sandcrete block consists of a mixture of cement and coarse sand mixed with water to obtain a normal consistency. The mix is then poured into a form and vibrated. Sandcrete structures may have a porosity of more than 25% depending on the extent of vibration. The sandcrete block forms the major construction material in the Nigeria building industry. Nigeria is a developing country. Pollution problems associated with heavy industrialization are today being experienced globally. However, all mitigating features to combat the trend

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of events have failed in the developing world as a result of these countries being converted to dumping grounds for used and inefficient machinery. Today no community is free from gaseous pollutants from automobiles and motorcycles manufactured using outdated technologies. Consequently, the major pollutants of our cities include products from incomplete burning of hydrocarbon fuel, such as  $\text{CO}_2$ ,  $\text{SO}_2$ ,  $\text{Cl}^-$ ,  $\text{CO}$ ,  $\text{NO}_x$ , etc. The presence of these pollutants has contributed not only to the depreciation of the peoples' quality of life, but also to the degradation of cement based structures' physicochemical, mechanical and aesthetic qualities [1].

These pollutants affect the properties of cement-based structures only when they are in direct contact. This is possible through adsorption and diffusion of these pollutants into the structure's matrix. Therefore, the rate of the pollutants' diffusion into the matrix will determine to a great extent the longevity of the cement-based structure. This is the focus of this research, with particular reference to long-serving sandcrete structures in Nigeria.

### 2.1. Basic assumption

The following assumptions were made to facilitate the derivation of the deterministic model equation.

1. The cement block is well compacted and therefore available inter pore space is assumed to be spherical if well compacted.
2. Fick's law holds for the diffusion mechanism.
3. The product of the chemical reaction is retained on the surface of the particles in a monomolecular layer.
4. Diffusion is predominantly in one direction of gas flow, except for particles at the edges.
5. The pollutant gases obey the general gas law
6. Surface flux is based on the total area of the solid particles perpendicular to the direction of diffusion.

By analogy to Fick's law, the molar rate per unit of pore surface  $N_s$  is (Eq. (1)) [6–8]

$$N_s = -D_s \frac{dC_s}{dr} \quad (1)$$

where  $C_s$  is the surface concentration (mol gas/ $\text{m}^3$ ) and  $r$  is the depth of pollutant gas penetration (m) [8].

For diffusion in a porous solid the surface flux  $(N_s)_e$  should be based on the total area perpendicular to the direction of diffusion on the coordinate  $r$

$$(N_s)_e = -\rho_b D_e \frac{dC_A}{dr} \quad (2)$$

where  $D_e$  is the effective diffusivity per unit of the total cross-sectional area,  $C$  the moles adsorbed per gram solid (mol/g) and  $\rho_b$  the density of the block.

The equilibrium concentration of the net rate of adsorption of gases on the solid, according to Langmuir's law can be represented as

$$C_A = K \bar{C}_m C_g \quad (3)$$

where  $C_A$  is the adsorbed concentration on the solid surface (mol/g),  $\bar{C}_m$  is the concentration corresponding to complete monomolecular layer on the solid,  $C_g$  the concentration of adsorbable component in the gas phase (it is proportional to  $P$ ) and  $K$  is the linear form of equilibrium constant ( $\text{m}^3/\text{g}$ ).

Due to the long exposure of the sandcrete blocks under investigation, equilibrium is assumed to exist between the gas and the surface concentration. Eq. (3) can be represented as

$$C_A = K_A \bar{C}_m C_g = K_A \frac{p y_A}{R_g T} \quad (4)$$

Substituting Eq. (4) into Eq. (2) gives Eq. (5).

$$(N_s)_e = -\frac{p}{R_g T} K_A D_e \rho_b \frac{dy_A}{dr} \quad (5)$$

The total surface flux is (Eq. (6))

$$(N_s)_t = N_s + (N_s)_e \quad (6)$$

Therefore

$$(N_s)_t = -\frac{p}{R_g T} (D + \rho_b K_A D_s) \frac{dy_A}{dr} \quad (7)$$

or

$$(N_s)_t = -(D + \rho_b K_A D_s) \frac{dC_A}{dr} \quad (8)$$

Therefore

$$(D_e)_t = D + \rho_b K_A D_s \quad (9)$$

The overall rate of reaction  $W_A$  of component A on the structure is (Eq. (10))

$$W_A = (N_A)_t V \quad (10)$$

where  $V$  is the volume of the structure = length  $\times$  width  $\times$  depth of pollutant gas penetration (LBr). Therefore, Eq. (8) becomes

$$W_A \frac{dr}{r} = -LB(D + \rho_b K_A D_s) dC_A \quad (11)$$

$$W_A \int_{r=0}^{r=r} \frac{dr}{r} = LB(D + \rho_b K_A D_s) \int_{C=C_A}^{C=0} dC_A \quad (12)$$

$$W_A \ln r = LB(D + \rho_b K_A D_s) C_A \quad (13)$$

Let  $LB$  = a constant and then assume that no diffusion took place, except on the perpendicular surface to the

direction of gas flow. In the linear form  $y=mx$ , Eq. (13) can be presented as

$$C_A = \frac{W_A}{D_c} \ln r \quad (14)$$

taking

$$D_c = LB(D + \rho_b K_A D_s)$$

where  $\ln r$  is the natural logarithm of the depth of pollutant gas penetration.

Eq. (14) is the modeling equation for the research.

### 3. Experiment

The samples A (20 years old) and B (15 years old) were collected from exposed long-serving sandcrete blocks used for fencing at highly industrialized layouts A and B in Lagos, Nigeria. The choice of samples was based on the age of the fence and centrality of the structure in the two industrial layouts. All samples were collected by drilling, using a hand-drilling machine, equal distances into the block wall used for the fence; at the top, middle and ground levels. The control sample (1 day old) was collected from a block industry in Minna; about 500 km north of Lagos. All samples were produced by mixing sand and cement with potable water. The mixture with moisture content of 30–40% is then poured into a mould and compressed either manually or vibrated mechanically. Minna is a city with practically no functional large-scale industry; consequently, except from automobiles and the homes, not many pollutants are generated. Each of the collected samples was ground in a ceramic-lined mill to a fineness of about 6–

8% residue on an 80- $\mu$ m-size mesh. All the chemical analyses were conducted according to Refs. [5,9].

### 4. Results and discussion

Results of the experiments are presented in Figs. 1 and 2 and Table 1. From Eq. (14),  $C_A$  is directly proportional to the natural logarithm of the depth of pollutant penetration,  $\ln r$ . The gradient of the line so obtained will be equal to  $W_A/D_c$ .  $W_A$  for a given pollutant is calculated from the quantity of reaction product deposited in the sandcrete over the experimental period. The results of analysis of the rate of reaction for the various pollutants are presented in Tables 2 and 3.

The  $\text{CO}_2$ ,  $\text{SO}_2$  and  $\text{Cl}^-$  were the pollutants investigated in this paper. Analysis, based on the quantity of deposition and rate of penetration, showed that the maximum concentration of the pollutants investigated ( $\text{SO}_2$ ,  $\text{CO}_2$  and  $\text{Cl}^-$ ) was dependent on the level and depth of sampling (Figs. 1 and 2 and Table 2). The concentration of  $\text{CO}_3^{2-}$  and  $\text{Cl}^-$  in the block increased by 3–10.5 and 1–2 times, respectively, over a 15- to 20-year period. The significant disparity in the  $\text{CO}_3^{2-}$  concentration maybe connected to the conversion of the insoluble  $\text{CaCO}_3$  to soluble  $\text{Ca}(\text{HCO}_3)_2$  and its subsequent leaching [2–4]. The concentration of  $\text{SO}_3$  increased by 1.6–6.5 times for sample A and 2.3–6.0 times for B in comparison to the control sample. The  $\text{Ca}(\text{OH})_2$  concentration during this 15–20 years decreased only by about 1.4 times for B and 1.3 for A. The mechanism of cement mineral hydration showed that the extent of hydration tends to 1 after many years [10]; with only about 60% extent of hydration attained after 180 days even for fast-hydrating cement [11]. The free  $\text{Ca}(\text{OH})_2$  is continuously utilized through various reactions such as in the

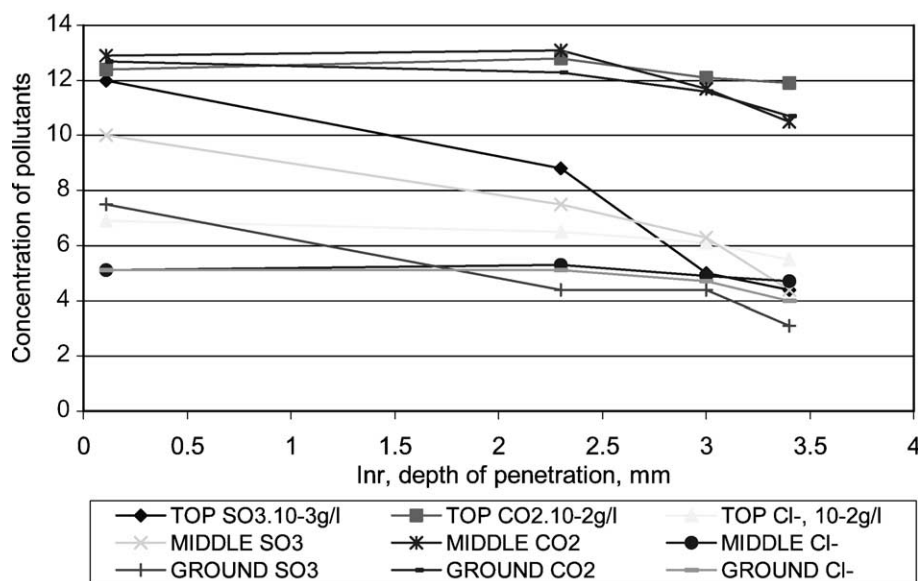


Fig. 1. Concentration of pollutants versus depth of penetration in Site A.

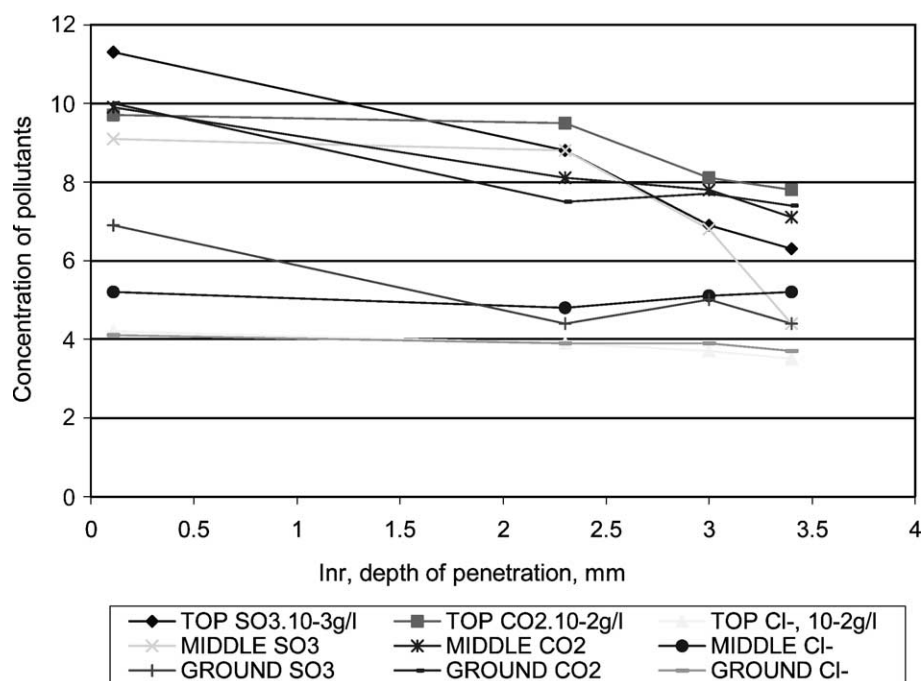


Fig. 2. Concentration of pollutants versus depth of penetration in Site B.

presence of  $\text{SO}_3$ , or  $\text{CO}_2$  or  $\text{Cl}^-$  and water to produce gypsum,  $\text{CaCO}_3$  ( $\text{Ca}(\text{HCO}_3)_2$ ) and  $\text{CaCl}_2$ , respectively. In the presence of active  $\text{SiO}_2$ ,  $\text{Ca}(\text{OH})_2$  will react to produce various solid solutions of C-S-H [11].

The porous nature of the sandcrete block ensures that the increased volume experienced as increased stress during the formation of ettringite in the course of the reaction involving  $\text{CaSO}_4 \cdot 2\text{H}_2\text{O}$  and calcium aluminate/ferrite hydrates is completely adsorbed. Unlike  $\text{SO}_2$  pollutant and sometimes  $\text{CO}_2$ ,  $\text{Cl}^-$  will always lead to increased porosity of the structure as the resultant soluble  $\text{CaCl}_2$  or unstable monochloroaluminates can be easily removed via leaching.

Analysis of Table 2 showed that the rate of deposition of all the pollutants investigated is higher at the outer surface. There is no linear relationship between the rate of reaction and the depth of the pollutants' penetration. The rate of deposition of  $\text{CO}_2$  in the sandcrete block was the highest irrespective of the depth or age of the samples. The  $\text{CO}_3^{2-}$  was fairly well distributed in all the depths investigated, with 4–25% variation between the outer and the inner layers. It is followed by  $\text{SO}_3$ ; however, the extent of variation was relatively high: 37% to 57%. The extent of

variation for  $\text{Cl}^-$  was the least. The difference in the various rates of reactions involving  $\text{SO}_2$ ,  $\text{Cl}_2$  and  $\text{CO}_2$  for samples A and B showed that the observed  $\text{Ca}(\text{OH})_2$  content (Table 1) could not have been the products of the primary reactions of cement minerals' hydration [10,11]. Their continuous presence is the resultant of various secondary reactions involving the cement minerals' hydrates and pollutants introduced into the sandcrete block.

Table 2  
Rate of various pollutants' deposition in sandcrete block

	Level					
Depth, $r$ (mm)	Top		Middle		Ground	
<i>Rate of <math>\text{SO}_3</math> deposition, <math>\times 10^{-9}</math> (g/l)/h at depths, for samples from sites A and B</i>						
0.9	69	87	59	72.5	44	53
10.0	50	67	43	67	25	33
20.0	28	53	36	48	25	38
30.0	25	48	25	33	17	33
<i>Rate of <math>\text{CO}_2</math> deposition, <math>\times 10^{-8}</math> (g/l)/h at depths, for samples from sites A and B</i>						
0.9	72	75	75	76	73	77
10.0	74	73	76	63	71	73
20.0	70	63	68	60	67	59
30.0	69	60	61	55	62	57
<i>Rate of <math>\text{Cl}^-</math> deposition, <math>\times 10^{-8}</math> (g/l)/h at depths for samples from sites A and B</i>						
0.9	40	49	3.0	40	30	32
10.0	38	46	3.1	37	30	30
20.0	35	46	2.8	39	27	30
30.0	32	45	2.7	40	23	29

Table 1  
Averaged concentration of  $\text{Ca}(\text{OH})_2$  at different depths

Depth, <i>r</i> (mm)	Sample concentration ( $\times 10^{-2}$ g/l)		
	Control	A	B
0.9	9.3	8.0	7.7
10.0	10.4	8.3	7.8
20.0	10.7	8.5	7.9

Table 3  
Diffusivity coefficients of pollutants in samples at different depths and levels

Depth, mm	Level					
	Top		Middle		Ground	
	A	B	A	B	A	B
<i>Diffusivity of SO<sub>3</sub>, × 10<sup>-6</sup> mm/h at depths, for samples from sites A and B</i>						
0.9–10	14.3	19.2	10.0	24.0	19.2	25.0
10–20	4.05	5.16	4.09	6.64	*	*
20–30	0.17	3.3	2.31	2.5	2.46	3.3
<i>Diffusivity of CO<sub>2</sub>, × 10<sup>-6</sup> mm/h at depths, for samples from sites A and B</i>						
0.9–10	*	25	*	17.3	11.8	3.84
10–20	4.0	5.0	4.0	7.0	4.0	4.83
20–30	0.5	4.0	2.3	2.86	2.22	2.66
<i>Diffusivity of Cl<sup>-</sup>, × 10<sup>-6</sup> mm/h at depths, for samples from sites A and B</i>						
0.9–10	12.0	25.0	*	10.0	*	25.0
10–20	5.88	*	5.26	*	5.26	*
20–30	2.0	2.0	3.3	*	2.28	2.0

\* Shows equilibrium or reverse in the relative rate of product deposition in the sandcrete depths. This retards the diffusivity of the pollutants.

The outer layer diffusivity values for all the pollutants investigated were, for most cases, higher than those of the interior (Table 3). However, the observed disparities of  $D$  values between the layers' depth might be connected with the nonuniform rates of leaching of the reaction products and the resultant exposure of the cement minerals' hydrates surfaces.

Among the pollutants investigated SO<sub>2</sub> has the highest  $D$  values; however, the high porosity of the sandcrete block structure coupled with the small percentage concentration in the mix made its degrading effect very minimal. The degrading effect of CO<sub>2</sub> was enhanced by its relative abundance in the atmosphere. The deposition of CaCO<sub>3</sub> on the outer surface of the sandcrete block reduces the penetration of CO<sub>2</sub> into the structure. The nonuniformity in the  $D$  values with increasing depth could be attributed to inconsistency in the diffusion of pollutant and the transformation of the resultant reaction product CaCO<sub>3</sub> to Ca(HCO<sub>3</sub>)<sub>2</sub> and the possible leaching from the structure. Chloride (Cl<sup>-</sup>) showed serious inconsistencies in the  $D$  values. This could be attributed to the relative ease with which the product of C-S-H and Cl<sup>-</sup> reaction is leached from the structure. The deterioration mechanism in the serving structure could therefore be considered dependent on the:

- In-built or self-destructive mechanism, which in this case include the quality of the cement, sand and water and the block production technique.
- External or prevailing environmental conditions and
- The extent of interaction of (a) and (b), to be defined by time.

These factors are adequately represented in the model Eq. (14). For any structure; even when serving in the same locality, the above-mentioned factors cannot be the same

due to variation in especially the internal factors. This could account for observed variations in data presented in Tables 2 and 3.

In general the study showed that the overall pollutants'  $D$  values in the sandcrete structure is dependent on the type of pollutant and its reaction with cement minerals, and the rate of leaching of these products. However, the developed mathematical model can serve as a comparative tool to determine the ease of diffusion of pollutants into the serving sandcrete block. The higher the diffusivity, the lesser will be the expected mechanical strength of the structure.

## 5. Conclusion

The developed model equation showed that intensive diffusion of pollutants takes place within 0–10 mm depth of the sandcrete block. It represents the relationship between the concentration of pollutant and depth of their penetration and gives a comparative measure of the ease of diffusion of the latter into the structure at various depths. Variation in the type of pollutant and possible reaction, including leaching, need to be considered in order to develop an acceptable model.

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