



# Microscopic effects on chloride diffusivity of cement pastes—a scale-transition analysis

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## Abstract

For estimation of the durability of structures, it is highly desirable to quantify and simulate the chloride diffusion process in concrete. To this end, diffusion–cell experiments delivering the chloride diffusivity of cement pastes with different water–cement ratios (related to different microporosities) are evaluated in a scale-transition analysis. For prediction of the apparent chloride diffusivity, cement paste can be modelled by means of a differential homogenization scheme involving nondiffusive spherical inclusions in a diffusive matrix. As a result, chloride diffusivity of cement paste is obtained as a function of the microporosity and the chloride diffusivity in the micropore solution. Remarkably, the latter turns out to be one order of magnitude smaller than the chloride diffusivity in a pure salt solution system. The smaller diffusivity is probably caused by structuring of water molecules along the pore surface of cement paste.

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**Keywords:** Chloride diffusion; Cement paste; Molecular water structuring; Scale transition; Multispecies transport

## 1. Introduction

One of the most severe durability problems in civil engineering is the deterioration of reinforced concrete structures through corrosion of the reinforcing steel. This process is accelerated by the possible presence of chloride which may be transported from the concrete surfaces (where it typically occurs as part of sea water or deicing salts on bridges) to the reinforcing steel. Thereby, chloride can be transported either together with water through the micropore space, driven by differences in the pore water pressure (advective transport), or chloride can diffuse through the pore water, driven by differences in the chloride concentration. Herein, we focus on the second form of transport. For estimation of the durability of structures, it is highly desirable to quantify and simulate this diffusion process. However, the chloride diffusivity through concrete and cement paste is characterized by a large variation, which depends strongly on the water–cement ratio [1–5]. Explan-

ations for this large variation and its chemophysical origin are still a matter of debate. The possible significance of an electric (diffuse) double layer on the one hand [6–8], and of multispecies ionic transport on the other [9–11], have been discussed, but no commonly accepted view has been established so far.

In this paper, we want to contribute to an explanation for the variation and the magnitude of chloride diffusivity in cement pastes. We evaluate numerous experimental data from cell–diffusion tests published in the open literature [1–5,12,13], in the framework of a scale-transition analysis [14,15] between the micropore-space scale and the cement-paste scale.

## 2. Diffusion–cell experiments for determination of chloride diffusivity of cement pastes

Steady-state chloride diffusion through water-saturated concrete and cement pastes is usually described by Fick's first law [1–5,13,16], e.g., in the form [17]:

$$\mathbf{J}_{\text{paste}} = -\mathbf{D}_{\text{paste}} \cdot \nabla c_{\text{paste}}, \quad (1)$$

where  $\mathbf{J}_{\text{paste}}$ ,  $\mathbf{D}_{\text{paste}}$ , and  $\nabla c_{\text{paste}}$  are the molar flux, the second-order diffusivity tensor, and the concentration gra-

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dient of sodium chloride in cement paste. Cement paste can be considered as isotropic material,  $\mathbf{D}_{\text{paste}} = \mathbf{1}D_{\text{paste}}$ , with the diffusion coefficient  $D_{\text{paste}}$ , and the second-order unity tensor  $\mathbf{1}$ .  $D_{\text{paste}}$  is commonly determined by diffusion–cell tests, where two cells, filled with solutions characterized by different salt concentrations, are separated by a cylindrical cement-paste sample with cross-sectional area  $A_{\text{sample}}$  and thickness  $t_{\text{sample}}$  (Fig. 1a). The concentration in the upstream (source) compartment,  $c_{\text{sol},1}$ , is kept constant during the experiment. In addition,  $c_{\text{sol},1}$  is chosen much larger than the salt concentration in the downstream (collector) compartment,  $c_{\text{sol},2}$ , i.e.,  $c_{\text{sol},1} \gg c_{\text{sol},2}$ . At the beginning of the test (see Fig. 1b),  $c_{\text{sol},2}$  is chosen to be virtually zero. The chloride ions need a certain time span to move into the downstream compartment. The end of this time span is indicated by an increase of  $c_{\text{sol},2}$  in the downstream compartment (see Fig. 1b). Monitoring  $c_{\text{sol},2}$  over time allows for estimation of the chloride flux,

$$J_{\text{paste}} = \frac{V_{\text{cell},2}}{A_{\text{sample}}} \frac{\Delta c_{\text{paste},2}}{\Delta t} \quad (2)$$

where  $V_{\text{cell},2}$  denotes the volume of the downstream cell. First,  $\Delta c_{\text{sol},2}/\Delta t$  is changing (Fig. 1b), so that transient conditions prevail. The duration of transient conditions increases with increasing thickness of the specimen. Afterwards, steady-state conditions (i.e.,  $\Delta c_{\text{sol},2}/\Delta t = \text{const}$ ) are observed. They allow for estimation of the chloride diffusion coefficient, based on the discrete 1D specification of Fick's first law for the diffusion–cell test,

$$J_{\text{paste}} = -D_{\text{paste}} \cdot \frac{\Delta c_{\text{paste}}}{\Delta x} = -D_{\text{paste}} \cdot \frac{c_{\text{paste},2} - c_{\text{paste},1}}{t_{\text{sample}}} \quad (3)$$

$D_{\text{paste}}$  can be expressed from Eq. (3) and Eq. (2), in the form:

$$D_{\text{paste}} = \frac{V_{\text{cell},2} \Delta c_{\text{paste},2}}{A_{\text{sample}} \Delta t} \frac{t_{\text{sample}}}{c_{\text{paste},1} - c_{\text{paste},2}}. \quad (4)$$

The chloride concentrations adjacent to the circular surfaces of the cement-paste sample,  $c_{\text{paste},i}$ ,  $i = 1, 2$ , can

Table 1

Curing conditions of cement paste diffusion experiments (P81 [1], Y91 [2], N95 [3], TN92 [4], Mc95 [5], ACP01 [51], C01 [12], H95 [13])

Number	Description of curing condition
i	Air curing at room temperature (90–100% relative humidity)
ii	Immersed in saturated $\text{Ca}(\text{OH})_2$ solution at room temperature
iii	Immersed in $\text{NaOH}$ solution at room temperature
iv	Immersed in $\text{H}_2\text{O}$ at room temperature

be determined from the chloride concentrations in the solutions of the upstream and the downstream cell,  $c_{\text{sol},i}$ ,  $i = 1, 2$ , and from the microporosity  $\phi$  of the cement-paste sample, through

$$c_{\text{paste},i} = \phi \cdot c_{\text{sol},i} \quad \text{with } i = 1, 2 \quad (5)$$

Insertion of Eq. (5) into Eq. (4) provides a relation for the determination of the diffusion coefficient of cement pastes from the physical properties accessible in diffusion–cell tests:

$$D_{\text{paste}} = \frac{V_{\text{cell},2} \Delta c_{\text{sol},2}}{A_{\text{sample}} \Delta t} \frac{t_{\text{sample}}}{c_{\text{sol},1} - c_{\text{sol},2}} \quad (6)$$

$D_{\text{paste}}$  is commonly referred to as apparent (or cement paste) diffusion coefficient, or more properly, as mass transfer coefficient [17]. In the literature dealing with chloride diffusion through cement paste, this coefficient is also denoted as ‘effective diffusion coefficient’ of cement paste (see, e.g., Refs. [1,5,12]). However, in geo-environmental engineering, a distinction is made between the effective and the apparent diffusion coefficient (see Ref. [18] for details). In the following, to avoid any confusion,  $D_{\text{paste}}$  will be referred to as apparent diffusion coefficient of cement paste.

Diffusion–cell tests are typically performed to explore the effects of variations of (i) the water–cement ratio [1,5], (ii) the curing conditions [19,20], and (iii) the sodium chloride concentration [1,5] (Tables 1, 2, and 3 and Fig. 2).

Whereas the influence of different curing conditions and of the sodium chloride concentration turns out to be of

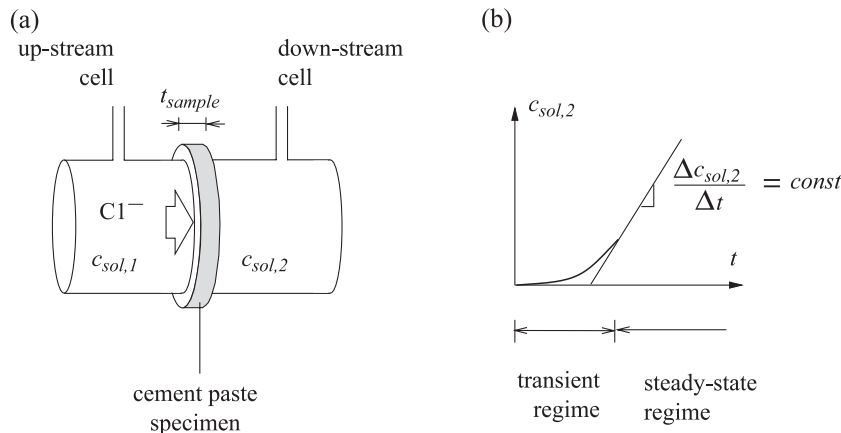


Fig. 1. Diffusion cell test: (a) schematical sketch; (b) time-dependent evolution of chloride concentration in downstream cell.

Table 2

Boundary conditions of cement-paste diffusion experiments (P81 [1], Y91 [2], N95 [3], TN92 [4], Mc95 [5], ACP01 [51], C01 [12], H95 [13])

Source	$c_{\text{sol},1}$ [mol/l]	$c_{\text{sol},2}$ [mol/l]	$t_{\text{cure}}$ [days]	$t_{\text{test}}$ [days]
P81	1 NaCl, Ca(OH) <sub>2</sub>	Ca(OH) <sub>2</sub>	60 <sup>i</sup>	21
Y91	1 NaCl, Ca(OH) <sub>2</sub>	Ca(OH) <sub>2</sub>	90–270 <sup>ii</sup>	21
N95	1 NaCl, 0.035 NaOH	0.035 NaOH	70 <sup>v</sup>	21
TN92	0.5 NaCl, Ca(OH) <sub>2</sub>	Ca(OH) <sub>2</sub>	90 <sup>ii</sup>	30
Mc95	0.5–4 NaCl	distilled H <sub>2</sub> O	56 <sup>i</sup>	125
ACP01	1 NaCl, 0.035 NaOH	0.035 NaOH	84 <sup>iii</sup>	
C01	1 NaCl, Ca(OH) <sub>2</sub>	Ca(OH) <sub>2</sub>	28 <sup>iv</sup> , 30 <sup>ii</sup>	21
H95	0.58 NaCl		60 <sup>iv</sup>	120

secondary importance, the strong functional dependence between water–cement ratio  $(w/c)_i$  and apparent diffusion coefficient  $D_{\text{paste}}$  is striking (Fig. 2 and Table 3). The chemo-physical origin of this dependence will be elucidated next, by performance and interpretation of a scale-transition analysis.

### 3. Evaluation of experiments by a scale-transition analysis

Diffusive transport of chloride (see Table 4 for ionic diameters) in a porous medium typically takes place in the pores of the material. For cement paste, different characteristic pore sizes motivate the distinction between micropores (‘capillary pores’ and ‘air pores’) on the one hand, and nanopores (‘gel pores’) on the other (Table 4). The rather large ratio of micropore diameter to the diameter of the ions encountered in cement paste (see Table 4) allows for a

Table 3

Experimental determination of composition and diffusivity of cement pastes:  $(w/c)_i$ =initial water–cement ratio (before curing), given in the literature;  $(w/c)_c$ =water–cement ratio after curing,  $(w/c)_c \geq 0.42$ ;  $\phi$ =solution-saturated porosity of cement paste;  $D_{\text{paste}}$ =apparent diffusion coefficient

Source	$(w/c)_i$ given	$(w/c)_c$ given ( $\geq 0.42$ )	$\phi$ Eq. (17)	$D_{\text{paste}}$ [ $10^{-12}$ m <sup>2</sup> /s] given or Eq. (6)
P81	0.40	0.42	0.065	2.600
	0.50	0.50	0.157	4.470
	0.60	0.60	0.249	12.35
Y91	0.35	0.42	0.065	1.200
	0.50	0.50	0.157	5.430
	0.60	0.60	0.249	7.300
N95	0.40	0.42	0.065	3.950
	0.50	0.50	0.157	7.800
	0.60	0.60	0.249	12.60
TN92	0.70	0.70	0.323	21.46
	0.40	0.42	0.065	2.900
	0.60	0.60	0.249	9.400
Mc95	0.80	0.80	0.384	21.00
	0.40	0.42	0.065	2.353
	0.50	0.50	0.157	6.412
ACP01	0.60	0.60	0.249	12.29
	0.70	0.70	0.323	18.73
	0.80	0.80	0.384	21.57
C01	0.35	0.42	0.065	0.40
C01	0.40	0.42	0.065	3.646
H95	0.55	0.55	0.206	11.25

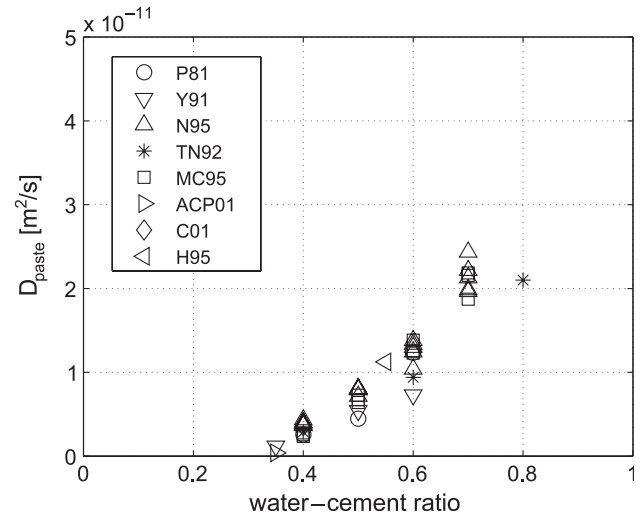


Fig. 2. Dependence of chloride diffusion coefficients of cement pastes  $D_{\text{paste}}$  on  $w/c$  ratio (P81 [1], Y91 [2], N95 [3], TN92 [4], Mc95 [5], ACP01 [51], C01 [12], H95 [13]).

continuum description of diffusive transport of chloride through the (saturated) pores. In cement paste, the diffusive transport of chloride ions takes place in the micropores [21] as long as they percolate, i.e., as long as they form a continuous pathway [22]. This is the common situation to which we refer herein. However, in case the micropores close off, diffusive transport of ions is accomplished through the much smaller nanopores [22].

We consider cement paste as a porous medium defined on a representative volume element (RVE) of some millimeters characteristic length  $\ell$  (Fig. 3).

This medium consists of two phases, schematically indicated in Fig. 3, a sodium-chloride-solution-filled micropore space and a solid phase consisting of aluminosilicate hydrates. While the solid phase is regarded as nondiffusive ( $D_{\text{solid}} \equiv 0$ ), we assign an average diffusion coefficient  $D_{\text{poresol}}$  to the pore fluid containing sodium chloride, presuming at this point the validity of Fick's first law in the micropore space

$$j_{\text{poresol}} = -D_{\text{poresol}} \nabla c_{\text{poresol}} \quad (7)$$

This equation holds at the length scale which is considerably smaller than that of the micropores,  $d$  in Fig. 3, and which is, at the same time, significantly larger than that of the

Table 4

Characteristic length scales of pores in cement paste and ions in solution

Pore type	$\phi$ Pores cement paste	Ion type	$\phi$ Ion unhydrated	$\phi$ Ion hydrated
Capillary	10 nm–100 $\mu\text{m}$ [53]	Na <sup>+</sup>	$2 \times 102$ pm [41]	$2 \times 250$ –330 pm [45]
	< 1 $\mu\text{m}$ [21]	K <sup>+</sup>	$2 \times 138$ pm [41]	$2 \times 180$ –200 pm [45]
Gel	< 10 nm [53]	Cl <sup>−</sup>	$2 \times 181$ pm [41]	$2 \times 200$ pm [45]
	< 2 nm [21]	OH <sup>−</sup>	$2 \times 25$ pm [41]	$2 \times 30$ pm [45]
Air	< 300 $\mu\text{m}$ [53]	H <sub>2</sub> O	–	0.28 nm [41]

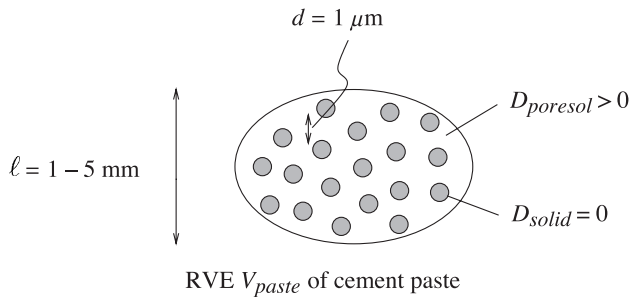


Fig. 3. Representation of cement paste as a two-phase material.

hydrated ions (see Table 4). At this scale, we are not aware of any measurement techniques for the estimation of  $D_{\text{poresol}}$ . As a first guess (the validity of which will be discussed later),  $D_{\text{poresol}}$  may be assumed to match the sodium chloride diffusion coefficient of a pure solution system, i.e.,  $D_{\text{poresol}} = 1.61 \times 10^{-9} \text{ m}^2/\text{s}$  [23] (see also Tables 5 and 6).

A micro–macro transition law relating  $D_{\text{poresol}}$  and  $D_{\text{paste}}$  is standardly given in the form [15,24] (pp. 1268, Eq. (9))

$$\mathbf{D}_{\text{paste}} = \phi D_{\text{poresol}} \mathbf{T}, \quad (8)$$

where  $\phi = V_{\text{pore}}/V_{\text{paste}}$  is the microporosity of cement paste ( $V_{\text{pore}}$  is the volume of micropores in the RVE with volume  $V_{\text{paste}}$ ); and the second-order ‘tortuosity tensor’  $\mathbf{T}$ , capturing geometrical information about the pore shape and arrangement (pore morphology). Accounting for the isotropy of the material,  $\mathbf{D}_{\text{paste}} = \mathbf{1} D_{\text{paste}}$ , Eq. (8) can be recast in the simpler form

$$D_{\text{paste}} = \phi D_{\text{poresol}} T \quad (9)$$

with the (dimensionless) tortuosity factor  $T$ . Alternatively, a (dimensionless) pore space topology factor (formation factor)  $\bar{F} = 1/(\phi T)$  is commonly introduced [25], resulting in a micro–macro transition law of the form

$$D_{\text{paste}} = \frac{D_{\text{poresol}}}{\bar{F}} \quad (10)$$

Without any further knowledge about the pore space except its porosity  $\phi$  and its isotropic nature, the tortuosity tensor  $\mathbf{T}$  can be suitably estimated using the so-called differential scheme of continuum micromechanics [15,26,27]. Based on Eshelby’s matrix inclusion problem [28], an infinitesimal amount of solid spherical inclusions is introduced into a matrix with  $D_{\text{poresol}}$ . The solid–fluid mixture is homogenized into a material with a well-defined diffusivity. This material serves as the matrix for the next infinitesimal amount of solid inclusions. This procedure is

Table 5

Salt diffusion (1:1 electrolytes, i.e.,  $z_+ = +1$ ,  $z_- = -1$ ) and self-diffusion coefficients (infinite dilute solution, according to Ref. [23])

Electrolyte	$D_{\text{sol}} [10^{-9} \text{ m}^2/\text{s}]$	$D_+ [10^{-9} \text{ m}^2/\text{s}]$	$D_- [10^{-9} \text{ m}^2/\text{s}]$
HCl	3.336	9.31	2.03
NaCl	1.610	1.33	2.03
KCl	1.994	1.96	2.03

Table 6

Salt diffusion coefficients at various concentrations at 25 °C (according to Ref. [23])

Concentration [mol/l]	$D_{\text{sol}} [10^{-9} \text{ m}^2/\text{s}]$		
	NaCl	KCl	HCl
0.05	1.507	1.864	3.07
0.1	1.483	1.844	3.05
0.2	1.475	1.838	3.06
0.5	1.474	1.850	3.18
1.0	1.484	1.892	3.43
1.5	1.495	1.943	3.74
3.0	1.565	2.112	4.65

repeated until the actual solid volume fraction ( $1 - \phi$ ) is reached, leading to the result [15]

$$\mathbf{T} = \phi^{1/2} \mathbf{1}, \quad (11)$$

$$\mathbf{D}_{\text{paste}} = \phi^{3/2} D_{\text{poresol}} \mathbf{1} \rightarrow D_{\text{paste}} = \phi^{3/2} D_{\text{poresol}} \quad (12)$$

Exactly the same result can be achieved by a differential effective medium approach for an assemblage of perfectly spherical grains [14], leading namely to  $\bar{F} = \phi^{-3/2}$  in Eq. (10).

Having thus gained confidence in the relevance of the micro–macro transition law Eq. (12), we want to confront this relation to experimental data. This requires determination of the water-saturated microporosity  $\phi$  from experiments.

Acker [29] has given the composition of cement pastes as a function of the water–cement ratio and the degree of hydration  $\xi$  (Fig. 4), reading as

$$\bar{V}_{\text{cem}}(\xi) = 1 - \xi \quad (13)$$

$$\bar{V}_{\text{H}_2\text{O}}(\xi) = \frac{\rho_{\text{cem}}}{\rho_{\text{H}_2\text{O}}} (w/c - 0.42\xi) \quad (14)$$

$$\bar{V}_{\text{hyd}}(\xi) = \frac{\rho_{\text{cem}}}{\rho_{\text{hyd}}} \xi. \quad (15)$$

Here,  $\langle \cdot \rangle$  represents the McAuley brackets,  $\langle x \rangle = 1/(2(x + |x|))$ .  $\rho_{\text{cem}} = 3.15 \text{ kg/dm}^3$ ,  $\rho_{\text{H}_2\text{O}} = 1.0 \text{ kg/dm}^3$ , and  $\rho_{\text{hyd}} =$

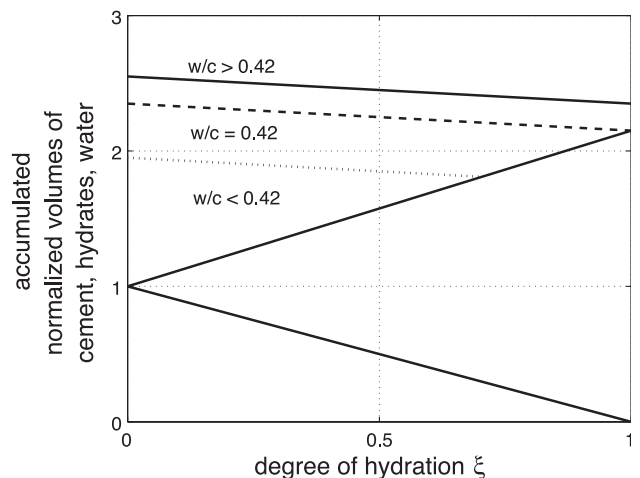


Fig. 4. Volumes of cement-paste components as a function of the degree of hydration, estimated according to Ref. [29].

1.46 kg/dm<sup>3</sup> [29] are the real mass densities of cement, water, and hydrates.  $\bar{V}_i$  stands for the volume of component  $i$  normalized with respect to the volume of cement at  $\xi=0$  (i.e., at the beginning of the hydration);

$$\bar{V}_i = V_i/V_{\text{cem}}(\xi=0) \rightarrow \bar{V}_{\text{cem}}(\xi=0) = 1 \quad (16)$$

(see also Fig. 4).

For  $w/c < 0.42$ , lack of water causes part of the cement to remain unhydrated ( $\xi_\infty < 1$ ; see dotted line in Fig. 4). However, all considered pastes with initial water–cement ratio  $(w/c)_i < 0.42$  (Fig. 4 and Table 2) were cured in water baths for at least 28 days (Table 2), so that they most probably attained a water–cement ratio of  $(w/c)_c = 0.42$  during curing. The duration of the curing period of all considered pastes, ranging between 28 and 270 days (Table 2), also suggests a complete hydration of the pastes at the end of the curing time,  $\xi_\infty = 1$ . Furthermore, water curing implies the filling of all original air pores (occupying normalized volume  $\bar{V}_{\text{air}}$ ) with water. This renders the volume fraction of the water-saturated micropores (or porosity  $\phi$ ) as the following function of the water–cement ratio:

$$\phi(w/c) = \frac{\bar{V}_{\text{air}}(\xi=1, w/c \geq 0.42) + \bar{V}_{\text{H}_2\text{O}}(\xi=1, w/c \geq 0.42)}{[\bar{V}_{\text{air}} + \bar{V}_{\text{H}_2\text{O}} + \bar{V}_{\text{hyd}} + \bar{V}_{\text{cem}}](\xi=1, w/c \geq 0.42)}, \quad (17)$$

where we make use of the relationships Eqs. (13)–(15). Respective porosity values for the data base depicted in Fig. 2 range between 7% and 38% (Table 3).

Experimentally determined data pairs  $(\phi, D_{\text{paste}})$  (Table 3) are largely overestimated by the theoretical relationship Eq. (12) if  $D_{\text{poresol}} = 1.61 \times 10^{-9} \text{ m}^2/\text{s}$  is assumed (see Fig. 5); that is, the simple guess of setting the pore solution

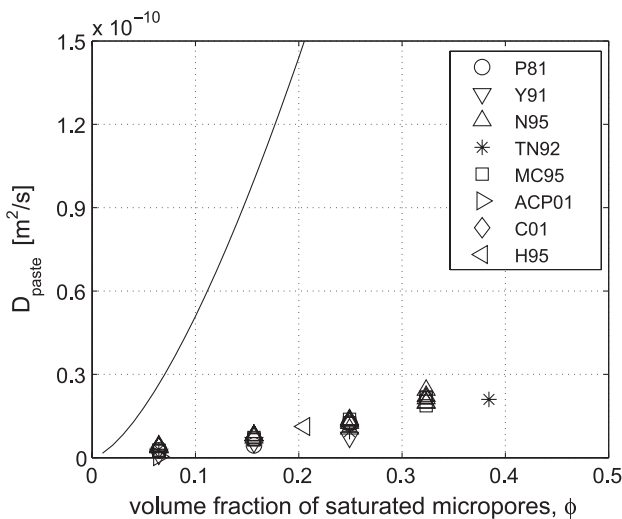


Fig. 5. Chloride diffusivity as a function of water-saturated porosity: comparison of experimental data (Table 3) and diffusion coefficients obtained by means of homogenization, Eq. (12) and  $D_{\text{poresol}} = 1.61 \times 10^{-9} \text{ m}^2/\text{s}$ .

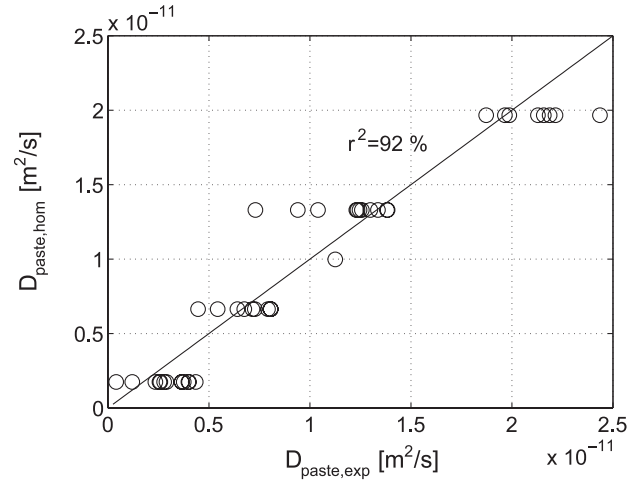


Fig. 6. Correlation of experimental data (Table 3) and diffusion coefficients obtained by means of homogenization, Eqs. (12) and (18).

diffusivity equal to the salt diffusivity in a pure solution system,  $D_{\text{NaCl}} = 1.61 \times 10^{-9} \text{ m}^2/\text{s}$ , turns out to be wrong.

However, what can also be seen is that the trend (shape) of the theoretical relationship fits very well with the one of the experiments. In fact, using a pore diffusion coefficient  $D_{\text{poresol,opt}} = 1.07 \times 10^{-10} \text{ m}^2/\text{s}$ , we get a high correlation coefficient of  $r^2=0.92$  (Fig. 6), between  $D_{\text{paste}}$  and  $D_{\text{paste,exp}}$ . This is an extraordinary correlation given the simplicity of the micro–macro transition law and of the relation for the estimation of the water-saturated porosity Eq. (17).  $D_{\text{poresol,opt}}$  was determined by minimizing the mean relative error between  $n=28$  experimental values  $D_{\text{paste},i}$  (Table 3) and homogenization results  $D_{\text{paste}}(\phi_i)$  from Eq. (12) (see Table 3 for the  $n$  values of  $\phi_i$ )

$$\bar{e} = \frac{1}{n} \sum \frac{D_{\text{paste},i} - (\phi_i)^{3/2} D_{\text{poresol}}}{D_{\text{paste},i}} \rightarrow \text{Min} \Rightarrow D_{\text{poresol,opt}} \quad (18)$$

In other words, using this optimized diffusion coefficient to describe the diffusive transport in the pore solution of cement paste results in an excellent agreement between experimental data and values of the homogenized diffusion coefficients (see Fig. 7). It is noteworthy that models not formulated in the framework of micromechanics generally merge information on the pore morphology and on the transport properties into a single parameter (see, e.g., Refs. [30,31]). This parameter must then be repeatedly determined for different experiments, characterized by, e.g., different  $w/c$  values (porosity values) and different pore solution compositions. The choice of  $D_{\text{poresol}}$  for this parameter, i.e., substituting  $\phi^{3/2}$  by  $\phi$  in Eq. (12), implies assumption of straight transport pathways of ions through the pores. Respectively determined paste diffusivity may be classified as Voigt upper bounds. As a rule, they strongly overestimate experimentally obtained apparent diffusion coefficients.

The surprising result in Figs. 6 and 7 is that the various experimental data could be reproduced well using a single



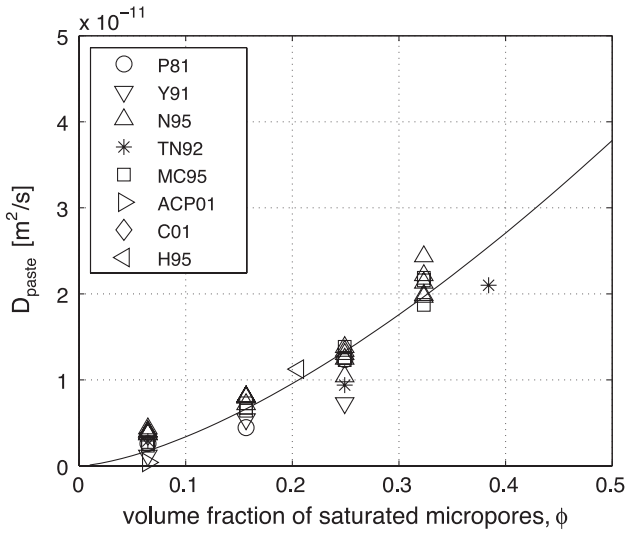


Fig. 7. Chloride diffusivity as a function of water-saturated porosity: comparison of experimental data (Table 3) and diffusion coefficients obtained by means of homogenization, Eqs. (12) and (18).

diffusion coefficient, i.e.,  $D_{\text{poresol,opt}}$  of the pore solution. The question now raised is, why the pore diffusion coefficient,  $D_{\text{poresol,opt}}$ , differs from the sodium chloride diffusion coefficient  $D_{\text{NaCl}}$  by a factor of 1/15. This question is addressed in the next section, but to this, some background understanding of multi-ion diffusion through a charged porous medium is first required.

#### 4. Discussion of chloride diffusion in the micropore space of cement pastes

To suggest a reasonable explanation for the magnitude of the pore space diffusion coefficient  $D_{\text{poresol,opt}}$  we determined previously, we have to precisely define the physical meaning of the diffusion coefficients  $D_{\text{paste}}$  (Eq. (1)) and  $D_{\text{poresol}}$  (Eq. (7)). For this reason, we give a short review of diffusive transport in pure liquids and charged porous media.

In a system consisting exclusively of a solution (pure solution system), four types of diffusion are commonly distinguished [18] (see Fig. 8): (i) self-diffusion, (ii) tracer diffusion, (iii) salt diffusion, and (iv) counterdiffusion.

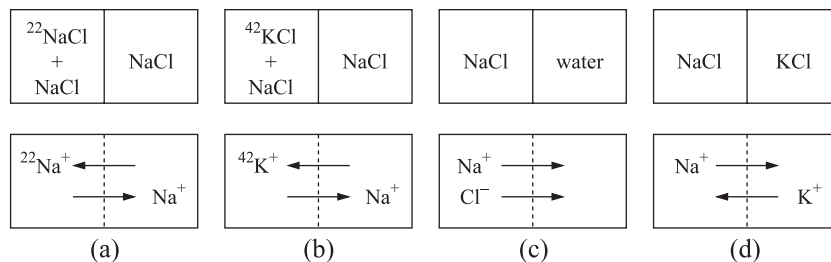


Fig. 8. Different types of diffusion: (a) self-diffusion, (b) tracer diffusion, (c) salt diffusion, and (d) counterdiffusion (according to Ref. [18]).

In case of dilute binary mixtures (one solute and one solvent), the first two types of diffusion (self-diffusion and tracer diffusion) can be described by Fick's first law [17]:

$$\mathbf{J}_i = -D_i \nabla c_i, \quad (19)$$

where  $\mathbf{J}_i$  denotes the molar flux density,  $D_i$  is the diffusion coefficient of the ion, and  $c_i$  is the concentration of ionic species  $i$ . Self-diffusion coefficients for anions and cations in infinitely dilute solutions (Table 5) are computed from the Einstein relation, i.e., from  $D_i = RTu_i$ , where the experimental values for the mobility  $u_i$  are extrapolated to zero concentrations.

For the description of salt diffusion, i.e., diffusion of dilute binary electrolytes [two (charged) solutes and one solvent], the Nernst–Planck (N–P) equation is required [32], reading for individual ions as:

$$\mathbf{J}_i = -D_i \left( \nabla c_i + \frac{F}{RT} z_i c_i \nabla \psi \right), \quad (20)$$

where  $F$  is the Faraday constant,  $z_i$  and  $D_i$  are the charge number and the self-diffusion coefficient of the  $i$ th ion,  $R$  is the universal gas constant,  $T$  is the absolute temperature, and  $\psi$  is the electric potential. The N–P Eq. (20) expresses that the ionic species  $i$  may be driven by a gradient of the electric field  $-\nabla \psi$  (migration) and/or by an ionic concentration gradient  $-\nabla c_i$  (diffusion). In the absence of net current flow (electroneutrality), the gradient of the electric potential can be expressed as [32]:

$$\nabla \psi = -\frac{RT}{F} \frac{D_+ - D_-}{z_+ D_+ - z_- D_-} \frac{1}{c_{\text{sol}}} \nabla c_{\text{sol}}, \quad c_{\text{sol}} = \frac{c_+}{v_+} = \frac{c_-}{v_-}, \quad (21)$$

where the subscripts  $+/-$  indicate cations and anions, respectively, and  $c_{\text{sol}}$  denotes the salt concentration.  $v_+$  and  $v_-$  are the stoichiometric coefficients of the cations and anions. Integration of Eq. (21) leads the diffusion potential (liquid junction potential) for a binary electrolyte, reading as:

$$\Delta \psi_L = -\frac{RT}{F} \frac{D_+ - D_-}{z_+ D_+ - z_- D_-} \ln \left( \frac{c_{\text{sol},2}}{c_{\text{sol},1}} \right). \quad (22)$$

Insertion of Eq. (21) into the N–P Eq. (20) delivers a steady-state diffusion equation for salts;

$$\mathbf{J}_{\text{sol}} = -D_{\text{sol}} \nabla c_{\text{sol}}, \quad (23)$$

where  $\mathbf{J}_{\text{sol}}$  and  $c_{\text{sol}}$  are the molar flux density and the concentration of the respective salt; and the salt diffusion coefficient  $D_{\text{sol}}$  has the form:

$$D_{\text{sol}} = \frac{D_+ D_- (z_+ - z_-)}{z_+ D_+ - z_- D_-} \quad (24)$$

(see Table 5). The mathematical similarity between Eq. (23) and Eq. (19) indicates that a salt solved in water behaves like a single ionic species, because of the electroneutrality requirement. In more detail, different self-diffusion coefficients of the anion and cation result in separation of the species. This leads to creation of a minute dipole density which then prevents further separation. The dipole density creates a potential (diffusion potential, Eq. (22)) which acts to speed up the ion with the smaller self-diffusion coefficients and slow down the ion with the larger self-diffusion coefficient.

Experiments show a dependence of salt diffusion coefficients on different concentrations (see Table 6). However, the diffusion coefficients of concentrated solutions (Table 6) and dilute solutions (Table 5) reasonably agree for concentrations up to 3.0 mol/l as far as NaCl and KCl solutions are concerned, and up to 1.0 mol/l for HCl solutions. Because we considered in our scale-transition analysis nondilute concentrations in the micropore solution which are smaller than 3 mol/l, (Table 2), the use of Fick's law Eq. (7) for the description of diffusive transport in the micropore space of cement paste is justified.

Still, with respect to pure solution systems, additional phenomena affect the diffusive transport in the micropores of cement, reducing the drift speed of chloride. The decrease of ionic drift speed in the pores may be attributed to (i) the presence of an (electrical) diffuse double layer (DDL) on particle surfaces, (ii) the presence of high concentrations of multiple ions in the pore solution, and (iii) changes of the viscosity of the pore solution caused by structuring of water. Let us more profoundly discuss these three possibilities:

- (i) Zeta potential measurements of cement pastes [33,34] indicate negative surface charges on cement-paste particles. The region where 'counterions' balance this excess charge is generally called electrical DDL [25]. It may be described by double- or triple-layer models (see, e.g., Ref. [35]). However, the presence of a DDL has been shown to *increase* (rather than decrease) the salt diffusivity [25]. At low salinity and/or high cation exchange capacity, there is a large difference in permeability for counterions (Na) and co-ions (Cl), a phenomenon called permselectivity. For a charged porous material at low salinity, the permselectivity increases the (absolute) value of the diffusion potential until its upper bound, which corresponds to the potential of a perfect membrane. The membrane potential increases the velocity of the co-ions to avoid generation of electric current. It follows that the macroscopic

diffusion coefficient is increased by this effect [25]. Consequently, the retardation of chloride ions cannot be attributed to the DDL. The DDL seemingly does not have a discernible effect on the chloride diffusivity of cement pastes at all, probably because of its compression due to salt concentrations around 1 mol/l NaCl, as was shown for platy clay soil [54].

- (ii) Experimental investigations of the cement pore solution have shown that the pore solution consists of multiple ions, such as  $\text{Na}^+$ ,  $\text{K}^+$ ,  $\text{Ca}^{2+}$ ,  $\text{OH}^-$ , and  $\text{SO}_4^{2-}$  ions [21,36–39]. While in this case, the ionic flux of each species can still be quantified by the N–P Eq. (20), the electric potential does not follow any more from Eq. (22), but from the more complex Henderson formula [40]

$$\Delta\psi_L = -\frac{RT}{F} \frac{\sum_{i=1}^N z_i D_i (c_{i,2} - c_{i,1})}{\sum_{i=1}^N z_i^2 D_i (c_{i,2} - c_{i,1})} \ln \left( \frac{\sum_{i=1}^N z_i^2 D_i c_{i,2}}{\sum_{i=1}^N z_i^2 D_i c_{i,1}} \right) \quad (25)$$

This formula allows for quantification of the effect of multiple ions on the chloride diffusivity, e.g., for a NaCl concentration ratio of  $c_{\text{sol},2}/c_{\text{sol},1} = 1:10$ , addition of ions, such as  $\text{Na}^+$ ,  $\text{K}^+$ , and  $\text{OH}^-$  in concentrations 150, 400, and 550 mol/m<sup>3</sup> to a 1-mol NaCl solution, resulting in a multispecies solution typical for cement pastes [11], which leads to a decrease of the (absolute value of) the diffusion potential from  $\psi_L = -12 \text{ mV}^1$  (for the NaCl solution Eq. (22)) to  $\psi_L = -3 \text{ mV}$  (for the multispecies solution Eq. (25)). This decrease and specification of the N–P Eq. (20) for chloride,  $z_{\text{Cl}} = -1$ , show that the presence of  $\text{Na}^+$ ,  $\text{K}^+$ , and  $\text{OH}^-$  leads to an acceleration (rather than to a retardation) of the chloride drift speed. Hence, judging from the diffusion potential, the decrease of chloride diffusivity in the saturated micropore space of cement pastes cannot be attributed to the presence of multiple ionic species.

A second characteristic of multispecies solutions is the smaller distance between ions, increasing the importance of ion–ion interactions. The presence of high concentrations of multiple ions in solution is standardly taken into account using activity coefficients [41] which describe the deviation of a solution from ideality. There are several theories for describing the relationship between activity coefficient and ionic concentration (strength) of the solution. Among these, the Pitzer model [42] and the extended Debye–Hückel model [43] are most commonly applied. However, application of the latter model for salt concentrations up to 1 mol/l at the pure solution level showed only a small variation of the salt diffusion coefficient,

<sup>1</sup> The diffusion potential is chosen as zero at the upstream side of the sample.

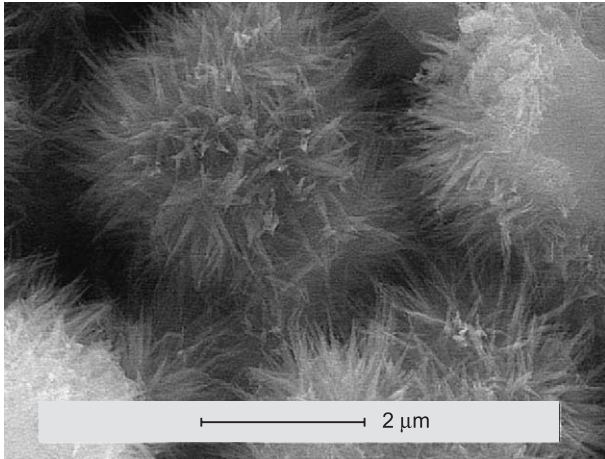


Fig. 9. Morphology of the cement-paste microstructure obtained from environmental scanning electron microscope (ESEM), 28 days after the onset of hydration (according to Ref. [52]).

typically between 4% (for NaCl and KCl solutions) and 8% (for LiCl solution, see Ref. [44] for details). Hence, the influence of additional ions in a multispecies solution seems inappropriate to explain the decrease of salt diffusivity in the micropores of cement pastes by the factor 1/15. This is in agreement with the numerical simulations of multispecies diffusion conducted in Ref. [11].

- (iii) Evidence has been put forward for almost one century that charged surfaces may imply structuring or layering of water (see Ref. [45] for a historical review). This phenomenon is known to occur in numerous materials, including, e.g., biopolymers [46]. In more detail, the polar nature of the water molecules leads to their absorption at the charged surfaces, constituting a first layer. Then, additional layers adhere one upon the other, forming a multilayered network. This layered network has physical properties which are distinctively different from standard liquid water; that is, the viscosity of layered water is significantly higher. Molecular dynamic (MD) simulations of a clay–salt water system show that the salt diffusion coefficient strongly depends on the viscosity of the pore solution [47,48]. While a viscosity of  $\mu_w = 0.001$  kg/(m s) leads to a diffusion coefficient of  $D_{\text{sol}} \approx 1.7 \times 10^{-9}$  m<sup>2</sup>/s, which is close to the one for a NaCl solution ( $D_{\text{sol}} = 1.61 \times 10^{-9}$  m<sup>2</sup>/s, see Table 5), an increase of viscosity to  $\mu_w = 0.007$  kg/(m s) leads to a diffusion coefficient of  $D_{\text{sol}} \approx 2.5 \times 10^{-10}$  m<sup>2</sup>/s. The latter value is of the same order of magnitude as the chloride diffusivity we determined for the pore solution of cement paste ( $D_{\text{poresol,opt}} = 1.1 \times 10^{-10}$  m<sup>2</sup>/s). The viscosity increase (and the diffusivity decrease, respectively) can be detected over a distance as large as several hundred nanometers [49]. The ‘spiny structure’ of cement paste at complete hydration (Fig. 9) [50] exhibits features of exactly this characteristic length.

This renders structuring of water as the prime candidate for the explanation of the decrease of chloride diffusivity in the micropore space of cement paste with respect to a pure salt solution.

## 5. Conclusions

For prediction of the apparent chloride diffusivity, cement paste can be modelled by means of a differential homogenization scheme involving nondiffusive spherical inclusions in a diffusive matrix. As a result, chloride diffusivity of cement paste is obtained as a function of the microporosity and the chloride diffusivity in the micropore solution. Remarkably, the latter turns out to be one order of magnitude smaller than the chloride diffusivity in a pure salt solution system. The smaller diffusivity is probably caused by a higher viscosity of the pore solution. This higher viscosity can be explained by the structuring of water molecules along the charged pore surfaces, a well-known phenomenon in clays and biological materials.

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## Appendix A. Notation

The following notation is used in this paper

$A_{\text{sample}}$	Area of cement-paste sample [m <sup>2</sup> ]
$c_i$	Concentration of ions in pure solution [mol/m <sup>3</sup> ]
$c_{\text{sol}}$	Sodium chloride ion concentration [mol/m <sup>3</sup> ]
$c_{\text{sol},1}, c_{\text{sol},2}$	Sodium chloride ion concentration in upstream and downstream compartment [mol/m <sup>3</sup> ]
$c_{\text{paste}}$	Sodium chloride ion concentration in cement paste [mol/m <sup>3</sup> ]
$c_{\text{poresol}}$	Sodium chloride ion concentration in pore solution of cement paste [mol/m <sup>3</sup> ]
$d$	Characteristic pore size [m]
$D_i$	Self-diffusion coefficient of ion $i$ [m <sup>2</sup> /s]
$D_{\text{sol}}$	Salt diffusion coefficient [m <sup>2</sup> /s]
$D_{\text{solid}}$	Sodium chloride ion diffusion coefficient of solid phase of cement paste [m <sup>2</sup> /s]
$D_{\text{paste}}$	Sodium chloride ion diffusion coefficient in cement paste [m <sup>2</sup> /s]
$D_{\text{paste,exp}}$	Experimentally determined sodium chloride ion diffusion coefficient in cement paste [m <sup>2</sup> /s]
$D_{\text{poresol}}$	Sodium chloride ion diffusion coefficient in pore solution of cement paste [m <sup>2</sup> /s]
$D_{\text{poresol,opt}}$	Sodium chloride ion diffusion coefficient in pore solution of cement paste obtained from optimization analysis [m <sup>2</sup> /s]
$D_{\text{NaCl}}$	Sodium chloride diffusion coefficient [m <sup>2</sup> /s]
$D_{\text{paste,hom}}$	Homogenized paste diffusion coefficient [m <sup>2</sup> /s]
$\bar{\epsilon}$	Relative error between homogenized and experimental diffusion coefficients



## Appendix A (continued)

$F$	Faraday constant $F=96,500$ [C/mol]
$\bar{F}$	Formation factor [–]
$\mathbf{j}_{\text{poresol}}$	Sodium chloride molar mass flux density in pore solution of cement paste [mol/(m <sup>3</sup> s)]
$\mathbf{J}_i$	Molar mass flux density of the $i$ th ion [mol/(m <sup>3</sup> s)]
$\mathbf{J}_{\text{sol}}$	Sodium chloride molar mass flux density in pure solution [mol/(m <sup>3</sup> s)]
$\mathbf{J}_{\text{paste}}$	Sodium chloride molar mass flux in cement paste [mol/(m <sup>3</sup> s)]
$\ell$	Characteristic length of representative volume element [m]
$n$	Number of experimental values of apparent diffusion coefficients
$R$	Universal gas constant $R=8.31$ [J/(K mol)]
$t_{\text{sample}}$	Thickness of cement-paste sample [m]
$\Delta t$	Time increment for diffusive transport [s]
$T$	Absolute temperature [K]
$T, \mathbf{T}$	Tortuosity factor, tortuosity tensor [–]
$u_i$	Ion mobility [(m <sup>2</sup> mol)/(J s)]
$w/c$	Water–cement ratio [–]
$(w/c)_i$	Water–cement ratio before curing [–]
$(w/c)_c$	Water–cement ratio after curing [–]
$(w/c)_{\text{exp}}$	Experimental water–cement ratio [–]
$V_{\text{paste}}$	Volume of cement paste [m <sup>3</sup> ]
$\bar{V}_{\text{air}}$	Volume of air pores normalized with respect to volume of cement at $\xi=0$ [–]
$\bar{V}_{\text{H}_2\text{O}}$	Volume of water normalized with respect to volume of cement at $\xi=0$ [–]
$\bar{V}_{\text{hyd}}$	Volume of hydrates normalized with respect to volume of cement at $\xi=0$ [–]
$\bar{V}_{\text{cem}}$	Volume of cement normalized with respect to volume of cement at $\xi=0$ [–]
$\Delta x$	Space increment for diffusive transport ( $x$ -direction) [m]
$z_i$	Charge number of the $i$ th ion [–]
$\nu_+, \nu_-$	Stoichiometric coefficients of cations and anions [–]
$\xi$	Degree of hydration [–]
$\rho_{\text{cem}}$	Mass density of cement [kg/m <sup>3</sup> ]
$\rho_{\text{hyd}}$	Mass density of hydrates [kg/m <sup>3</sup> ]
$\rho_{\text{H}_2\text{O}}$	Mass density of water [kg/m <sup>3</sup> ]
$\phi$	Capillary porosity of cement paste [–]
$\phi_{\text{exp}}$	Experimental capillary porosity of cement paste [–]
$\phi_{\text{exp},i}$	Experimental capillary porosity of $i$ th experiment [–]
$\psi$	Electric potential [V]
$\Delta\psi_L$	Diffusion potential [V]

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